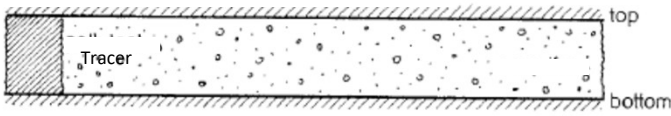


Sorption

Exercise 1: Breakthrough Curve

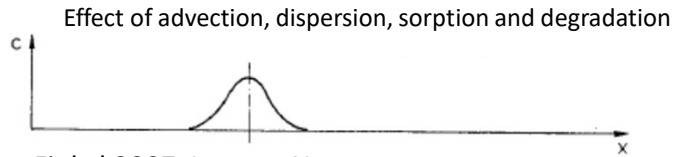
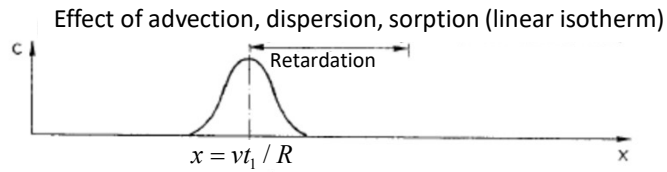
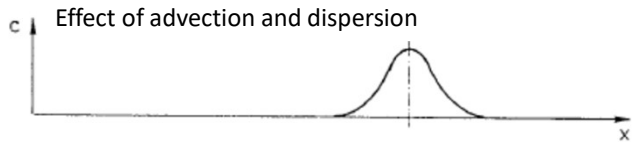
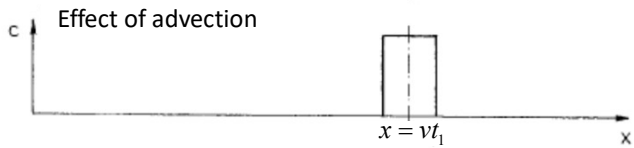
Concentration Distribution at time t=0



A pulse injection



Concentration Distribution at time t_1 > 0



Finkel 2007, Lecture Notes

$$\frac{\partial c}{\partial t} = -v \frac{\partial c}{\partial x}$$

$$\frac{\partial c}{\partial t} = -v \frac{\partial c}{\partial x} + D \frac{\partial^2 c}{\partial x^2}$$

$$R \frac{\partial c}{\partial t} = -v \frac{\partial c}{\partial x} + D \frac{\partial^2 c}{\partial x^2}$$

$$R \frac{\partial c}{\partial t} = -v \frac{\partial c}{\partial x} + D \frac{\partial^2 c}{\partial x^2} + r_w + \frac{(1 - n_e)}{n_e} r_s$$

A Sorbing Phase

The mass fluxes are not affected by sorption, but the solute can also be stored in the solid phase. The volumetric water content is the effective porosity n_e and the volumetric content of solids is $(1-n_e)$. The new mass balance with a solid sorbing phase:

$$m = [n_e c_w + (1 - n_e) c_s] A \Delta x$$

$$\frac{\partial c}{\partial t} = -v \frac{\partial c}{\partial x} \quad \frac{\partial}{\partial t} (n_e c_w + (1 - n_e) c_s) = -q \frac{\partial c_w}{\partial x} \quad \frac{\partial}{\partial t} \left(c_w + \frac{(1 - n_e)}{n_e} c_s \right) = -v \frac{\partial c_w}{\partial x}$$

One thing to note is that Sorbing compounds are often quantified as mass fraction s [$M_{\text{solute}}/M_{\text{solid}}$] in the solid. ρ_s [M_{solid}/L^3] is the density of the solids.

$$c_s = \rho_s s$$

$$\frac{\partial}{\partial t} \left(c_w + \frac{(1 - n_e)}{n_e} \rho_s s \right) = -v \frac{\partial c_w}{\partial x}$$

A Sorbing Phase: Equilibrium

Only when we assume that sorption is at equilibrium at any point within the domain, the relationship between the two concentrations is unique with functional relationship $f(c_w(x))$ known as sorption isotherm

$$s(x) = f(c_w(x))$$

Advective transport equation

$$\frac{\partial}{\partial t} \left(c_w + \frac{(1-n_e)}{n_e} \underbrace{\rho_s s}_{c_s} \right) = -v \frac{\partial c_w}{\partial x}$$

Advective transport with a sorbing phase

$$R \frac{\partial c_w}{\partial t} = -v \frac{\partial c_w}{\partial x}$$

Using chain-rule

$$\frac{\partial c_s}{\partial t} = \frac{\partial c_w}{\partial t} \frac{\partial c_s}{\partial c_w}$$

$$\frac{\partial}{\partial t} \left(c_w + \frac{(1-n_e)}{n_e} c_s \right) = \underbrace{\left(1 + \frac{(1-n_e)}{n_e} \frac{\partial c_s}{\partial c_w} \right)}_{R(c)} \frac{\partial c_w}{\partial t}$$

How to define the sorption isotherm for the retardation factor R ?

It depends whether you have

- Linear sorption
- Non-linear sorption

Retardation Factor: Linear Equilibrium Sorption

$$\frac{\partial}{\partial t} \left(c_w + \frac{(1-n_e)}{n_e} c_s \right) = \underbrace{\left(1 + \frac{(1-n_e)}{n_e} \frac{\partial c_s}{\partial c_w} \right)}_{R(c)} \frac{\partial c_w}{\partial t} \quad c_s = \rho_s s$$

$$s(x) = f(c_w(x))$$

$$s = K_d c_w$$

K_d [L^3/M_{solid}] is partitioning coefficient between the solid and the aqueous phase.

What is the retardation factor for linear equilibrium sorption?

$$R = 1 + \frac{(1-n_e)}{n_e} \rho_s K_d$$

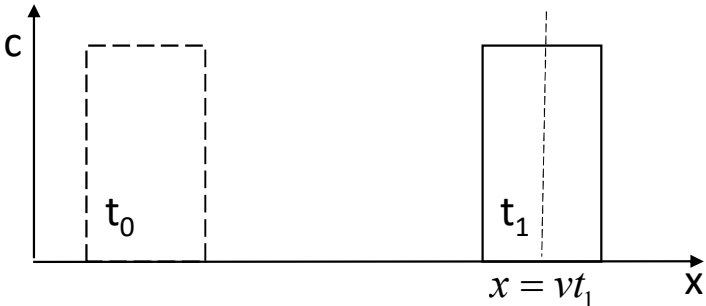
$$K_d = K_{oc} f_{oc}$$

K_{oc} [L^3/M_{Corg}] partitioning coefficient between organic carbon and water
 f_{oc} [-] fraction of organic carbon.

Retardation Factor: Linear Equilibrium Sorption

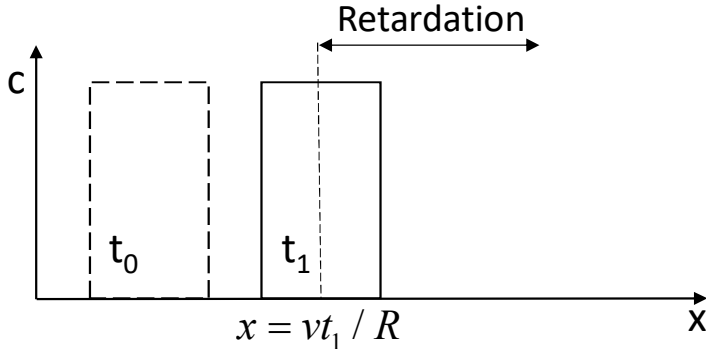
Advection

$$\frac{\partial c}{\partial t} = -v \frac{\partial c}{\partial x}$$



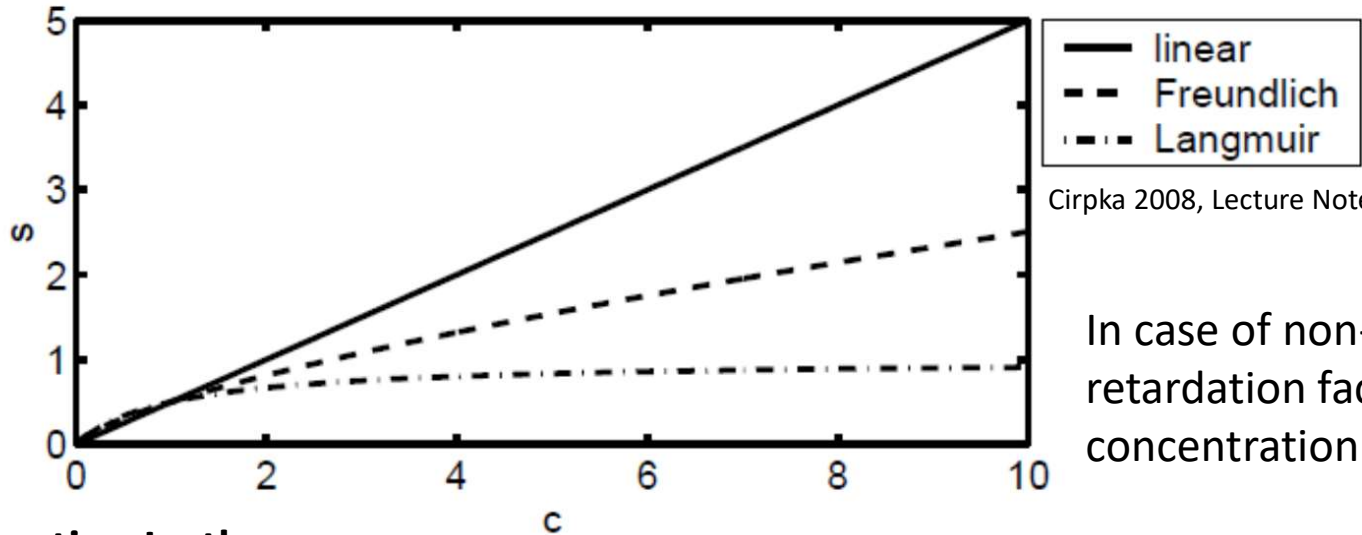
Advection+ Linear Sorption

$$R \frac{\partial c_w}{\partial t} = -v \frac{\partial c_w}{\partial x}$$



For linear sorption at equilibrium: the non-retarded and retarded concentration profiles are identical. The only difference is that everything happens at later time.

Retardation Factor: Non-Linear Equilibrium Sorption



In case of non-linear sorption, the retardation factor depends on the concentration

Sorption Isotherm

$$s(x) = f(c_w(x))$$

$$s(x) = K_d c$$

$$s(x) = K c^n$$

$$s(x) = \frac{s_{\max} K}{c + K}$$

Retardation factor

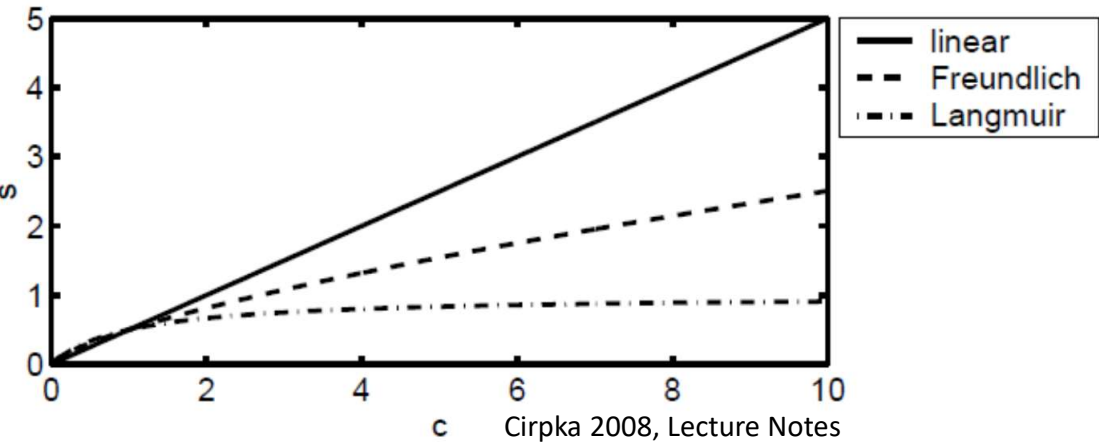
$$R = 1 + \frac{(1 - n_e)}{n_e} \rho_s K_d$$

$$R = 1 + \frac{(1 - n_e)}{n_e} \rho_s K n c^{n-1}$$

$$R = 1 + \frac{(1 - n_e)}{n_e} \rho_s \frac{s_{\max} K}{(c + K)^2}$$

How non-linear sorption affect breakthrough curves?

How Non-Linear Sorption Affect Breakthrough Curve?

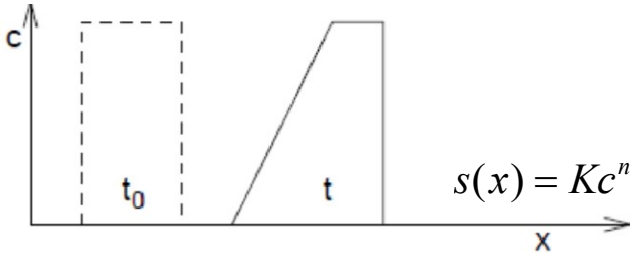
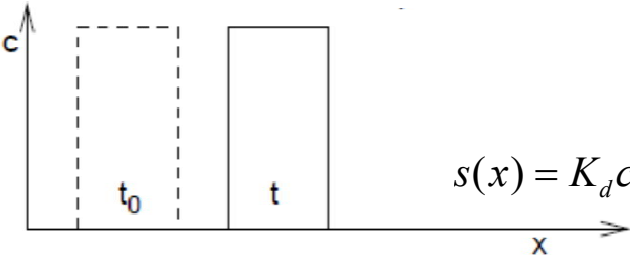
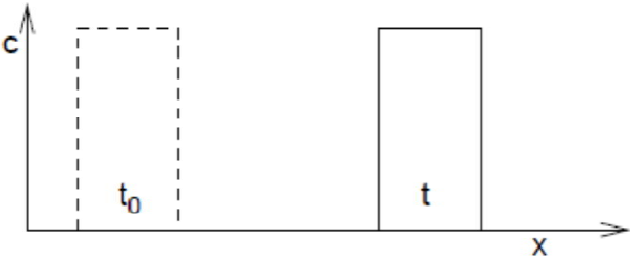


Cirpka 2008, Lecture Notes

How non-linear sorption affect breakthrough curves?

- Concentration changes are slowed down more dramatically at lower concentrations than at higher concentrations.
- This leads to a deformation of the concentration profiles with sharp front and stronger retardation at smaller concentrations.

Non-linear sorption: the retardation factor depends on the concentration



Exercise 2: Retardation Factor

Can the retardation become factor $R < 1$?

Name	Sorption Isotherm	Retardation Factor
Linear	$s(c) = K_d c$	$R = 1 + \frac{(1 - n_e)}{n_e} \rho_s K_d$
Freundlich	$s(c) = K c^n$	$R = 1 + \frac{(1 - n_e)}{n_e} \rho_s K n c^{n-1}$
Langmuir	$s = \frac{s_{\max} K}{c + K}$	$R = 1 + \frac{(1 - n_e)}{n_e} \rho_s \frac{s_{\max} K}{(c + K)^2}$

Note that for Langmuir sorption isotherm: S_{\max} [$M_{\text{solute}}/M_{\text{solid}}$] is the sorption site density generally reported in mol/kg, and K [M/L^3] is the half-saturation concentration at which the sorbed concentration s equals exactly 50% of its maximum value.

A retardation factor $R < 1$, implies $K < 0$, which is not physically possible.